

1 *Article*

2 **Removal of Eutrophication Agents from Wastewater Using Glauconite-Based**
3 **Sorbents**

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21

22 **Abstract:** Excessive phosphorus and nitrogen in water and sediment may cause eutrophication,
23 which poses a potential risk to drinking water safety and the sustainability of aquatic ecosystems.
24 The research focuses on the removal of phosphates and ammonium ions from aqueous solutions
25 using a new thermally and microwave-treated glauconite. The surface morphology of the samples
26 was studied by SEM. BET surface area, pore volume, and pore size distribution were measured.
27 Adsorption studies were carried out in static and dynamic conditions. The best fit for adsorption of
28 the both pollutants is given by Langmuir-Freundlich and BET models. The calcined sample
29 showed the lowest adsorption capacity for phosphate but the highest capacity for ammonium.
30 Conversely, for the microwave-irradiated sample, the adsorption capacity for phosphate increases,
31 while that for ammonium remains at the same level. In dynamic conditions phosphorus was most
32 efficiently retained by natural glauconite, and ammonium nitrogen by glauconite that was ther-
33 mally treated in a muffle furnace.

34 **Keywords:** glauconite; adsorption; eutrophication agents; water pollution; thermal treatment;
35 microwave irradiation.

36 **1. Introduction**

37 Water pollution is one of the main environmental issues that has released contaminating
38 substances into fresh water bodies or groundwater [1]. Natural water sources are polluted by un-
39 treated or insufficiently treated wastewater [2]. Variety of methods and technologies is developed
40 for wastewater treatment. Usually, wastewater is treated using activated sludge microorganisms or
41 chemical reagents. Conventional methods effectively remove organic matter from wastewater, but
42 it is not possible to remove phosphorus completely [3]. Nitrogen is another threatening biogenic
43 element that escapes into the environment with wastewater [4]. In recent years, there has been a
44 significant focus on the advancement of new technologies for environmental protection (5-8).
45 Excessive P and N in water and sediment can cause eutrophication, which poses a potential risk to
46 drinking water safety and the sustainability of aquatic ecosystems [5]. Effective removal of
47 phosphorus and nitrogen from wastewater is therefore a key strategy to control eutrophication. The

48 final stage of technological processes should be additional treatment with sorbent materials [9].
49 Adsorption technology is the most widely used technology for wastewater treatment [6, 10-13].
50 The simplicity of design, speed, efficiency, and profitability determine the wide use of sorbents
51 [14]. Commercially available sorbents are rather expensive, which significantly limits the range of
52 their application areas [15]. In this context, natural clay mineral adsorbents can be used as an
53 alternative [14]. Natural adsorbents are inexpensive, environmentally friendly, and available in
54 large quantities [7, 13]. Natural silicates possessing high adsorption, ion exchange, molecu-
55 lar-sieve, and catalytic characteristics deserve special attention [15-18]. Often, nitrogen in
56 wastewater is in the ammonium form, so it can be removed by ion exchange. Ammonium ions are
57 effectively removed from water or wastewater by zeolites [19, 20]. Most clay minerals produce a
58 net negative surface charge due to the isomorphic substitutions of Si (IV) by Al (III) or Fe (III) [1].
59 Iron-based materials exhibit high efficiency for P immobilization due to their strong affinity with P
60 [5]. The Fe-rich sorbents can effectively immobilize P in sediment under oxic conditions through
61 adsorption and/or precipitation [8, 21]. However, not all natural clays are suitable for wastewater
62 treatment. Bauxite and olivine are not applicable due to the presence of significant amounts of lead
63 and/or nickel [22]. For wastewater treatment, the big interest is represented by natural sorbents
64 which concern glauconite. It can primarily be used as a long-term organic fertilizer because the
65 potassium, iron, and phosphorus present in glauconite pass into the soil and improve its properties
66 [23]. High efficiency glauconite is demonstrated at the clarification of water from salts of heavy
67 metals, some organic and inorganic structures, and radionuclides [18, 24]. Galangashi et al. used
68 glauconite to remove ammonium ions from water and found that ion exchange was the main
69 mechanism for ammonium removal [25]. The efficiency of sorption in the mineral rock of various
70 deposits is determined to a large extent by the content of granular glauconite in it, as well as by the
71 presence of iron oxide in the composition [15]. The advantages of this mineral are as follows: wide
72 circulation, cheapness, availability, granular structure, thermal stability, good ion exchange, and
73 filtration properties [5]. Due to these properties, glauconite can be applied to environmental

74 technologies [26, 27]. Glauconite is a natural aluminosilicate, dioctahedral micaceous phyllosilicate
75 mineral. It is an aqueous aluminosilicate of iron, silica, and potassium oxide of unstable compo-
76 sition. The final composition can vary depending on the origin of the mineral and affect its sorp-
77 tion properties [5, 15]. Clay minerals are considered the most effective adsorbents, but the modi-
78 fication methods can improve the capacity, capability, and selectivity of the adsorption properties
79 of clays [1]. Modification processes such as acid activation, heat treatment, column, organic
80 functionalization are used to obtain the desired properties [28-30]. Microwave irradiation has
81 proven successful in preparing new promising materials for water treatment by causing structural
82 and textural changes that enhance the products' adsorption capacity [9, 31]. Sorptive capacity is an
83 important parameter that allows evaluation of the durability of the sorbent material. It is deter-
84 mined during mixing tests. However, a unified methodology for determining the sorption capacity
85 of aggregates has not yet been developed. For this reason, researchers obtain different values of the
86 sorption capacity of the same aggregates. On the other hand, only a few studies have been focused
87 on real wastewater treatment.

88 This research focuses on the removal of phosphates and ammonium ions from aqueous
89 solutions using a new thermally and microwave-treated glauconite. A new method of glauconite
90 modification was proposed, samples modified in several ways were produced and tested, and their
91 properties were compared with the properties of natural glauconite. This work aimed to identify
92 the physicochemical characteristics of Ukrainian glauconite and assess its sorption properties for
93 extracting ammonium ions and phosphates from wastewater.

94 **2. Materials and methods**

95 *2.1. Characterization of adsorbents*

96 According to the related literature [32-34], heat treatment of sorbents can harden the
97 structure and increase their sorption capacity. The initial sample of glauconite (pH of aqueous
98 extract – 8.6; bulk density – 1049,85 kg/m³) was sieved to obtain a particle size fraction of 0.8-1.2

99 mm. To improve the performance characteristics of glauconite, it was pre-treated with the fol-
100 lowing methods: calcination at 550 °C for 3 hours, and microwave treatment for 30 min at 790 W.

101 *2.1.1. SEM and EDS*

102 The surface morphology of the powdered samples was studied by scanning electron mi-
103 croscopy (SEM). The qualitative and quantitative composition of the samples was determined
104 using energy dispersive X-ray spectroscopy (EDS) on a Tescan Vega3 LMU electron microscope
105 equipped with the advanced Oxford Instruments Aztec ONE system (CCD Si drift detector
106 X-MaxN20). Before the study, the sample powders were applied to an electrically conductive film.
107 The experiments were performed at a W-cathode voltage of 20-25 kV. The SE detector charac-
108 terizes the surface morphology and details its irregularities, while the BSE detector shows the
109 contrast of phases with different element fillings.

110 *2.1.2. BET surface area and pore size distribution*

111 Before starting the measurement, the samples were placed in a vacuum and degassed at 150
112 °C for 3 hours. BET surface area, pore volume, and pore size distribution of the studied sorbents,
113 as well as nitrogen adsorption/desorption isotherms, were recorded by Quantachrome Auto-
114 sorb-iQ-KR/MP automated, high-vacuum, gas sorption analyser. Measurements of nitrogen ad-
115 sorption and desorption isotherms were conducted at -196 °C (77 K). The specific surface area was
116 calculated by the BET (Brunauer–Emmett–Teller) equation. The density functional theory (DFT)
117 and QSDFT method were applied for making the pore size distribution plot. The total pore volume
118 was determined from the adsorption isotherm by measuring the amount of nitrogen adsorbed at a
119 relative pressure of $p/p_0 = 0.99$. All calculations were performed using the ASiQwin program
120 (Version 2.0), developed by Quantachrome Instrument.

121 *2.2. Experiments methodology*

122 *2.2.1. Adsorption isotherms*

123 The sorption properties of the samples were investigated under static conditions. Batch
124 experiments were conducted at room temperature for a 24-hour period.

125 Anhydrous salts KH_2PO_4 and NH_4Cl were used for preparing the model PO_4^{3-} and NH_4^+
126 solutions respectively. The working solutions were prepared from the initial solutions by repeated
127 dilution with distilled water. The PO_4^{3-} concentration was determined by KFK-2 photoelectric
128 colorimeter. For the measurement of NH_4^+ content, the Ionometer AI-125 was used.

129 The experimental results were fitted to the following three isotherm models:

130 - the Langmuir-Freundlich isotherm model [35]:

131

$$132 \quad q_e = \frac{q_m(K_{LF}C_e)^{n_{LF}}}{1+(K_{LF}C_e)^{n_{LF}}} , \quad (1)$$

133

134 where q_e and C_e are and the equilibrium concentration in solid and liquid phases, respec-
135 tively. q_m is the adsorption capacity. K_{LF} is the affinity constant, and n_{LF} is the coefficient of het-
136 erogeneity or a measure of the adsorption intensity.

137 - the Dubinin-Radushkevich model [36] :

138

$$139 \quad q_e = q_m \exp^{-Be^2} , \quad (2)$$

140

141 where B is the model's constant, and e – Polanyi potential.

142 - the BET model [37]:

143

$$144 \quad q_e = \frac{q_m C_{BET} C_e}{(C_e - C_S) \left[1 + (C_{BET} - 1) \frac{C_e}{C_S} \right]} , \quad (3)$$

145

146 where C_{BET} is and constant of the model, and C_S is f concentration of solute at the moment
147 of saturation of all layers.

148 The nonlinear modelling was carried out according to procedure described in our previous
149 works [38].

150 2.2.2. Breakthrough curves

151 Domestic wastewater (which had already been biologically treated in an individual plant)
152 was filtered on a laboratory bench (Fig. 1):

153

154 **Figure 1.** Laboratory bench with three columns

155

156 The wastewater was filtered (filtration rate 5 ml/min) through three columns, which were
157 filled as follows:

158 Column 1: supporting layer of pebbles; 7 cm high layer of quartz sand; mixed filler ("4"
159 glauconite (Glauconite for 3 hours in a muffle furnace at a temperature of 550 °C) plus 60 g of
160 quartz sand), 20 g of quartz sand.

161 Column 2: supporting layer of pebbles; 7 cm high layer of quartz sand; mixed filler ("3"
162 glauconite (Natural glauconite) plus 60 g of quartz sand), 20 g of quartz sand.

163 Column 3: supporting layer of pebbles; 7 cm high layer of quartz sand; mixed filler ("5"
164 glauconite (Glauconite 30 min under the influence of microwaves) plus 60 g of quartz sand), 20 g
165 of quartz sand.

166 The filtration experiment lasted 4 hours. Filtrate samples were taken hourly for ammonium
167 nitrogen and phosphate phosphorus concentration.

168 The initial concentration of PO₄-P in the wastewater was 4.85 mg/L; and the initial con-
169 centration of NH₄-N was 16.1 mg/l.

170 The effectiveness of removing PO₄-P from wastewater was calculated according to for-
171 mula (4):

$$172 \quad E_i = \frac{(C_{1i} - C_{2i})}{C_{1i}} \cdot 100, \quad (4)$$

173 where: E_i – effectiveness of removing $PO_4\text{-P}$, %; $C_{1,i}$ – concentration of $PO_4\text{-P}$ before
174 treatment, mg/L; $C_{2,i}$ – concentration of $PO_4\text{-P}$ after treatment, mg/L. The study was repeated two
175 more times to present the mean results of three experiments.

176 MERCK Spectroquant® tests were used to determine the phosphorus concentration of
177 phosphates. Test limits 0.50-30.0 mg/l $PO_4\text{-P}$. Absorbance measurements of the test solution were
178 performed by pouring test samples into 10 mm cuvettes (Hellma) and measuring at the required
179 wavelength (410 nm) with a Genesys 10 UV–Vis spectrophotometer (Thermo Fisher Scientific,
180 USA). MERCK Spectroquant® tests were used to determine ammonium nitrogen concentration.
181 Test limits 2.0-75.0 mg/l $NH_4\text{-N}$. Absorbance measurements of the test solution were performed
182 after 15 minutes by pouring test samples into 10 mm cuvettes (Hellma) and measuring at the
183 required wavelength (690 nm) with a Genesys 10 UV–Vis spectrophotometer (Thermo Fisher
184 Scientific, USA).

185 3. Results and discussion

186 3.1. SEM and EDS

187

188 **Figure 2.** SEM images of glauconite (SE detector on the left, BSE detector on the right): a
189 - initial sample, b - calcined at 550 °C, c - microwave irradiated

190 Fig.2 shows the surface morphology of powdered samples of natural glauconite. The size
191 of the crystallites of the original sample is 2-20 microns. The shape of the grains is similar to
192 blocks with cut edges. The peculiarity of the stacking of these blocks is significant aggregation
193 between them, probably due to crystallization water.

194 Heat or microwave treatment changes both the grain shape and morphology of the sample.
195 Large aggregates of ~20 μm crack into smaller fragments (5-10 μm) with a highly developed
196 surface during processing. In the case of thermal treatment, spherical particles can be observed

197 next to the blocky grains. On the surface of each particle, we can see microcracks, which con-
198 tribute to further amorphization of the sample as the processing time increases. A similar effect is
199 observed for the sample after microwave treatment. The evaporation of crystallization water
200 causes the formation of micropores and microcracks and increases the surface area of the grains
201 for further sorption of ammonium (NH_4^+) and phosphate (PO_4^{3-}) ions.

202 The overall composition of the sample does not undergo significant changes, as water is
203 mainly released during the treatment. Some changes are due to the heterogeneity of the composi-
204 tion of natural glauconite. Fig. 3 shows the elemental distribution on the sample surface. The ratio
205 of cations for the original sample is Na/Mg/Al/Si/K/Ca/Ti/Fe
206 1.17/1.07/13.39/74.41/4.45/4.00/0.35/1.16. The elemental ratios for the muffle furnace-annealed
207 and microwave-irradiated samples are Mg/Al/Si/K/Ca/Fe 5.20/11.35/59.90/7.82/3.30/12.43 and
208 Mg/Al/Si/K/Ca/Fe 5.76/11.52/58.36/7.42/4.09/12.85, respectively.

209

210 **Figure 3.** Elemental distribution on the surface of glauconite

211 a - initial sample, b - calcined at 550 °C, c - microwave irradiated

212

213 *3.2. Surface area and porosity*

214 The N_2 adsorption-desorption isotherms for natural and modified samples are presented in
215 Fig.4. Due to hysteresis loops present on the plot of the samples we assume that the materials are
216 mesoporous. The hysteresis loops in all the isotherms are of type IV (IUPAC) with the loops of the
217 H3 type [39]. The H3 type is characterized by the presence of wedge-shaped pores, resulting from
218 the loose arrangement of flaky particles. It is evident on the micrographs of the test samples
219 (Fig. 4).

220

221 **Figure 4.** N_2 adsorption-desorption isotherms

222 The results of porosimetry are presented in Table 1. The equivalent particle size (d_{part}) was
223 estimated using the relation (5) [40]:

224

$$225 \quad d_{part} = \frac{6000}{S_{BET} \cdot \rho}, \quad (5)$$

226

227 Where ρ is the density of bulk composite in g/cm^3 and S_{BET} is expressed in m^2/g . The po-
228 rosity of the particles (ε) is calculated using the following equation (6) [41]:

229

$$230 \quad \varepsilon = \frac{V_p}{V_p + 1/\rho_{app}}, \quad (6)$$

231

232 Where V_p is the pore volume (cm^3/g) and ρ_{app} is the apparent density (g/cm^3) of investi-
233 gated materials.

234 It was found that high-temperature treatment reduces the BET surface area from 54.99 to
235 43.57 m^2/g . In contrast, under the influence of microwave irradiation, the surface area changes
236 much less. However, an interesting fact was the increase in the external surface area of the glau-
237 conite sample under the influence of microwave irradiation with a simultaneous decrease in the
238 micropore area. Whereas calcination at 550 °C causes only a decrease in the micropore surface
239 area (Fig. 5). Expectedly, the equivalent particle size increases under the influence of high tem-
240 perature due to sintering from 103.9 to 156.7 nm.

241 **Table 1.** Specific surface area (S_{BET}), micropore area (S_{mic}), external surface area (S_{ext}), pore
242 volume (V_p), equivalent particle size (d_{part}), and porosity (ε) of natural and modified clinoptilolite.

243

244 **Figure 5.** Pore size distribution

245 *3.2. Adsorption isotherms*

246 The results of the nonlinear fitting of experimental research within theoretical models are
247 presented in Tables 2 and 3.

248

249 **Table 2.** NH_4^+ adsorption isotherms nonlinear fitting parameters.

250 **Table 3.** PO_4^{3-} adsorption isotherms nonlinear fitting parameters.

251

252 The best fit for adsorption of the both pollutants is given by Langmuir-Freundlich model,
253 but it doesn't provide any information about the adsorption mechanism. In order to identify the
254 physical or chemical mechanism of adsorption the Dubinin-Radushkevich isotherm was used.
255 From the determination of the average free energy of adsorption (E), the nature of the process can
256 be inferred. The calculated values of E in all studied cases are less than 8 kJ/mol, so the adsorption
257 process is of physical nature. Meanwhile the BET model also fits well to experimental data. This
258 model describes the physical adsorption process rather well and allows the formation of n layers.
259 The adsorption isotherms of NH_4^+ and PO_4^{3-} on natural and modified clinoptilolite are presented
260 in Fig. 6 and 7 respectively.

261

262 **Figure 6.** Isotherms of NH_4^+ adsorption

263 **Figure 7.** Isotherms of PO_4^{3-} adsorption

264

265 The shapes of the curves are quite different. The isotherm of NH_4^+ adsorption corresponds
266 to Type-IV according to the IUPAC classification [46], while the PO_4^{3-} isotherm corresponds to
267 the Type-V. According to [42], Type-V isotherms are related to microporous materials, as opposed
268 to the Type-VI isotherm where multilayer adsorption occurs on a uniform non-porous surface [43].
269 Therefore, it can be assumed that NH_4^+ is absorbed by the external surface of the samples, but
270 phosphate ion is well fixed in the micropores. This coincides with the results of the porosity study

271 of the samples before and after treatment. As shown in Table 1, heat treatment at high temperatures
272 leads to a significant decrease in microporosity by 42.3%. Therefore, it is the calcined sample that
273 shows the lowest adsorption capacity for phosphate. In contrast, this increases the adsorption
274 capacity of the sample for ammonium. Conversely, for the microwave-irradiated sample, the
275 adsorption capacity for phosphate increases, while that for ammonium remains at the same level.

276 *3.3. Breakthrough capacity*

277 Fig. 8 clearly demonstrates that, in the initial two hours, both the natural and micro-
278 wave-irradiated samples exhibited superior effectiveness of PO_4^{3-} removal compared to the
279 thermally treated sorbent. 3 hours later, all three samples reached almost the same retention rate.
280 The best result in terms of phosphate uptake was shown by the natural glauconite and slightly
281 worse by the microwave irradiated sample. Thermal modification significantly worsens the sorp-
282 tion properties of glauconite for phosphate. Thus, in the case of phosphate absorption under dy-
283 namic conditions, heat treatment of glauconite does not lead to a significant improvement in
284 sorption properties.

285

286 **Figure 8.** $\text{PO}_4\text{-P}$ retention efficiency

287

288 A completely opposite phenomenon is observed in the ammonium absorption. As can be
289 seen from Fig. 9, the highest removal rate during the first hour is demonstrated by the natural and
290 heat-treated samples. However, subsequently, the ammonium retention efficiency begins to de-
291 crease sharply for both the natural and microwave irradiated samples. At the same time, the
292 heat-treated sorbent continues effectively purifying water (more than 80% efficiency) even after 3
293 hours of exposure. Thus, in the case of ammonium nitrogen purification, heat treatment of glau-
294 conite significantly improves its sorption capacity.

295

296 **Figure 9.** $\text{NH}_4\text{-N}$ retention efficiency

298 Hence, phosphate phosphorus and ammonium nitrogen retention took place in all columns.
299 Phosphorus was most efficiently retained by natural glauconite, and ammonium nitrogen by
300 glauconite that was calcinated in a muffle furnace for 3 hours at 550 °C. In general, all three
301 columns removed ammonium nitrogen more efficiently than phosphate phosphorus.

302 **4. Conclusions**

303 New thermally and microwave-treated glauconite for removal of eutrophication agents
304 (phosphate phosphorus and ammonium nitrogen) from aqueous solutions was investigated.

305 SEM-EDS investigation revealed that heat or microwave treatment changes both the grain
306 shape and morphology of the sample. Large aggregates of ~20 µm crack into smaller fragments
307 (5-10 µm) with a highly developed surface during processing. The evaporation of crystallization
308 water causes the formation of micropores and microcracks and increases the surface area of the
309 grains for further sorption of ammonium (NH_4^+) and phosphate (PO_4^{3-}) ions. Heat and microwave
310 treatment of glauconite causes similar changes in the cation ratio.

311 Measurements of the BET surface area showed that high-temperature treatment leads to its
312 reduction. However, it is important to note that this decrease is primarily attributed to the reduction
313 in micropore surface area. Whereas the increase in the external surface area of the glauconite
314 sample under the influence of microwave irradiation is accompanied by a decrease in the micro-
315 pore area.

316 The best fit for the adsorption isotherm of both pollutants is given by Langmuir-Freundlich
317 and BET models. The values of average free energy calculated from Dubinin-Radushkevich model
318 were less than 8 kJ/mol, so the adsorption process is of a physical nature. The shapes of the
319 phosphate and ammonia adsorption isotherms are quite different. The shape of PO_4^{3-} isotherm is of
320 the type related to microporous materials, as opposed to the type of NH_4^+ isotherm where multi-
321 layer adsorption occurs on a uniform non-porous surface. Therefore, it can be assumed that NH_4^+

322 is absorbed by the external surface of the samples, but phosphate ion is well fixed in the micro-
323 pores. This coincides with the results of the porosity study of the samples before and after treat-
324 ment. Moreover, it is the calcined sample that shows the lowest adsorption capacity for phosphate
325 but the better adsorption capacity for ammonium. Conversely, for the microwave-irradiated
326 sample, the adsorption capacity for phosphate increases, while that for ammonium remains at the
327 same level.

328 The best result in phosphate uptake in dynamic conditions was shown by the natural
329 glauconite and slightly worse by the microwave-irradiated sample. Thermal modification sig-
330 nificantly worsens the sorption properties of glauconite for phosphate. A completely opposite
331 phenomenon is observed in the ammonium absorption. The highest removal rate during the first
332 hour is demonstrated by the natural and heat-treated samples. However, subsequently, the am-
333 monium retention efficiency begins to decrease sharply for both the natural and micro-
334 wave-irradiated samples. At the same time, the heat-treated sorbent continues effectively purifying
335 water (more than 80% efficiency) even after 3 hours of exposure. Thus, in the case of ammonium
336 nitrogen purification, heat treatment of glauconite significantly improves its sorption capacity. In
337 general, all three columns removed ammonium nitrogen more efficiently than phosphate phos-
338 phorus.

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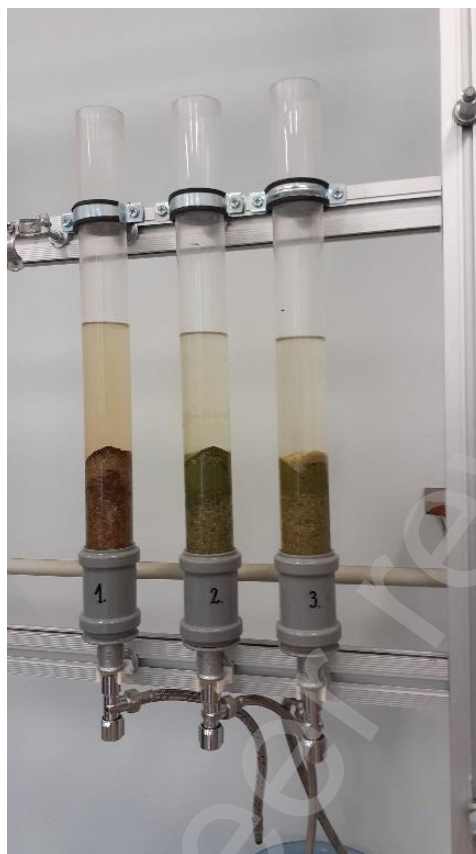
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Figure 1. Laboratory bench with three columns



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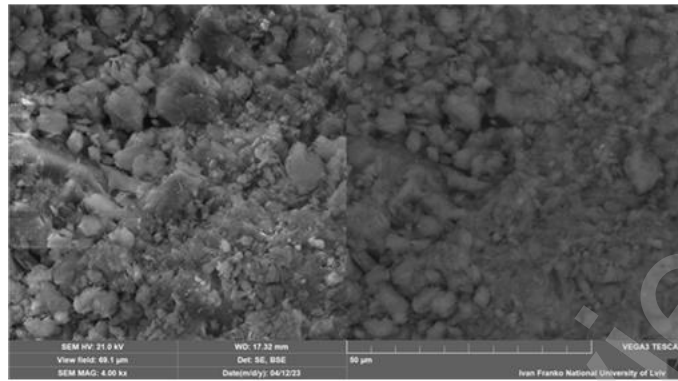
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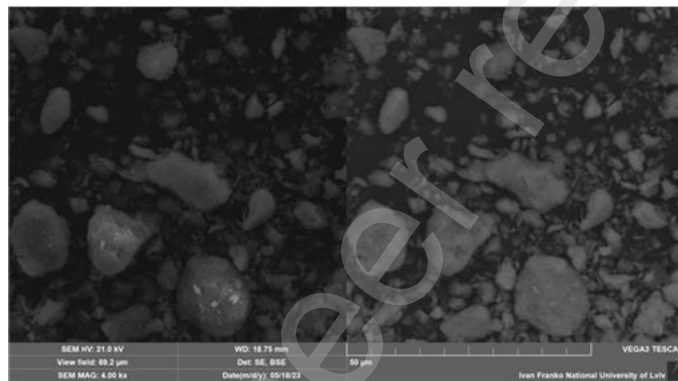
Figure 2. SEM images of glauconite (SE detector on the left, BSE detector on the right): a

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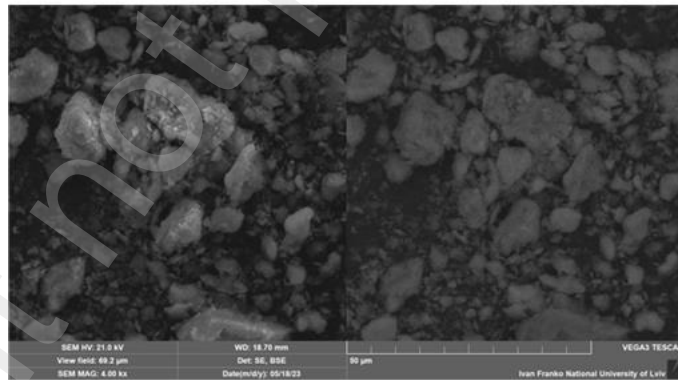
- initial sample, b - calcined at 550 °C, c - microwave irradiated



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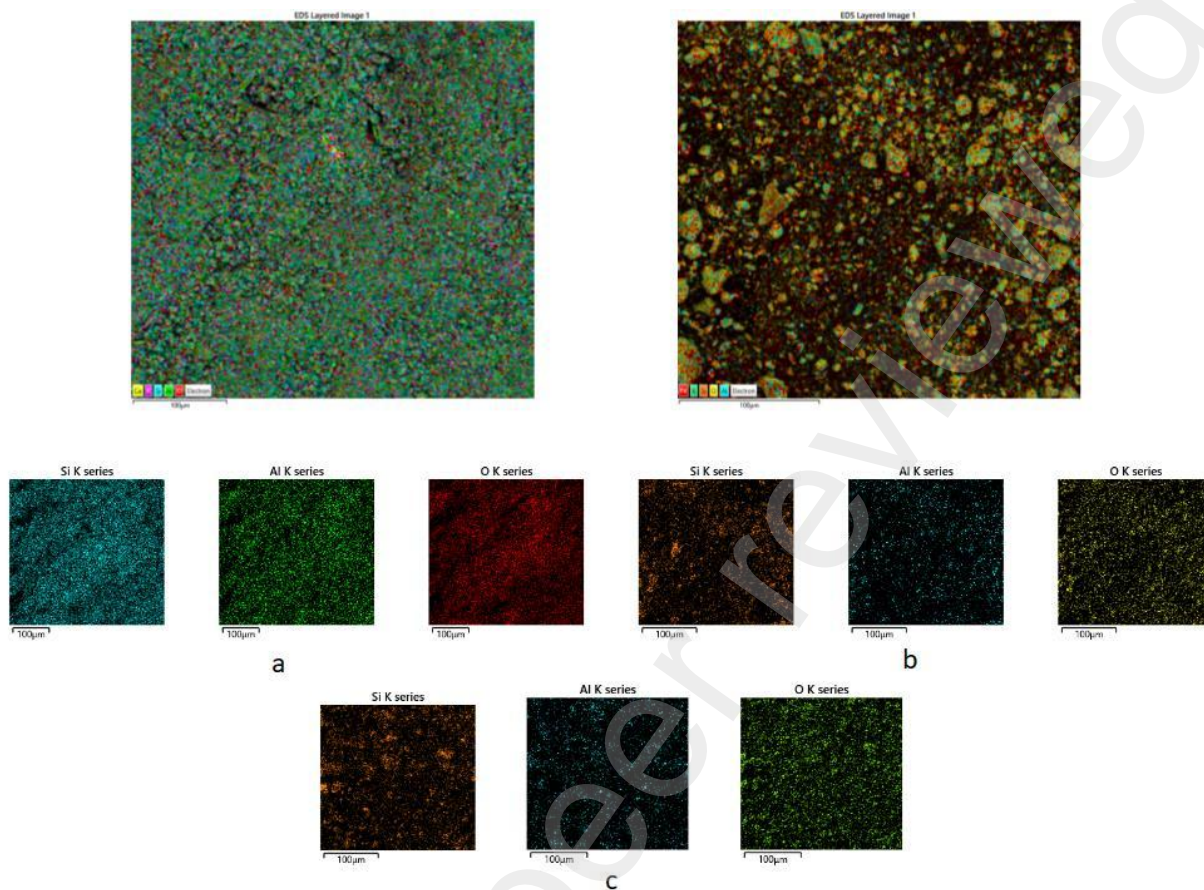
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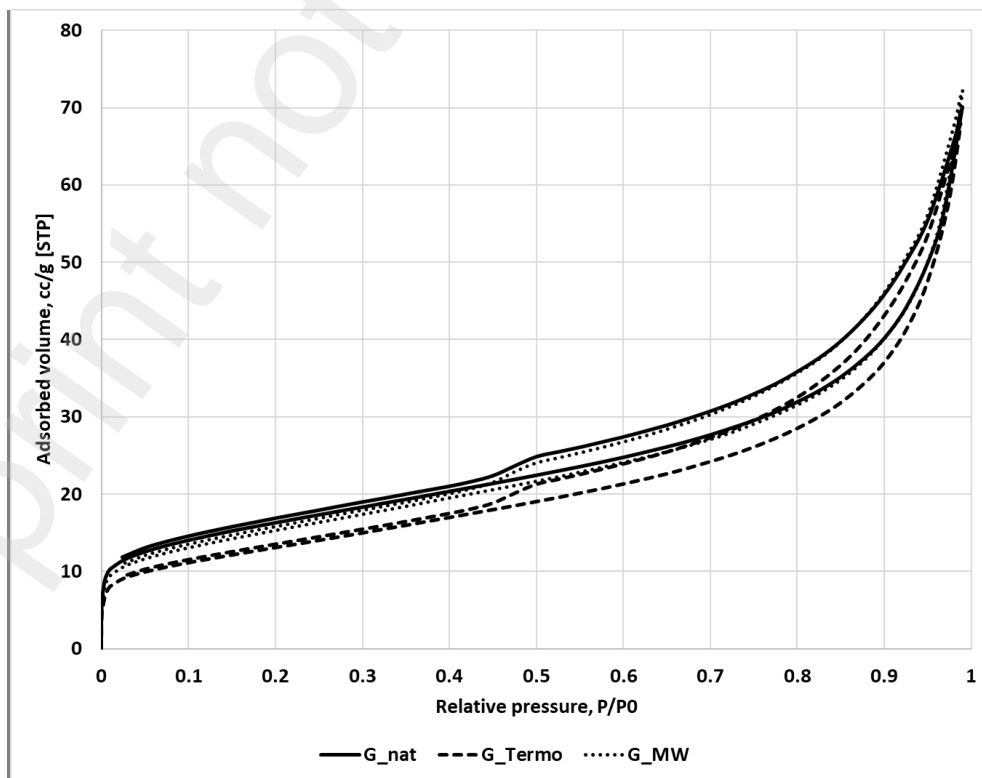
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Figure 3. Elemental distribution on the surface of glauconite
a - initial sample, b - calcined at 550 °C, c - microwave irradiated



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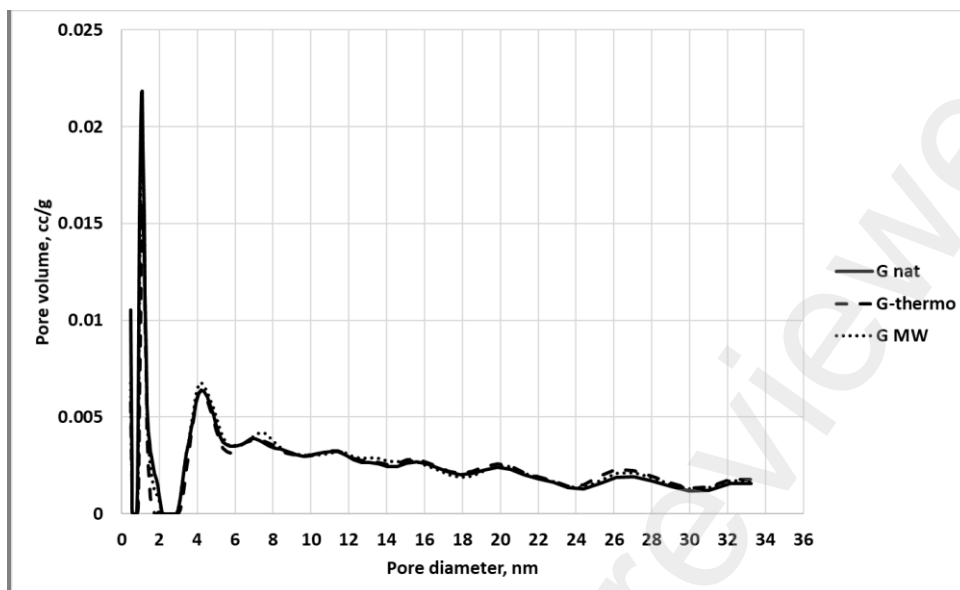
Figure 4. N₂ adsorption-desorption isotherms



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Figure 5. Pore size distribution

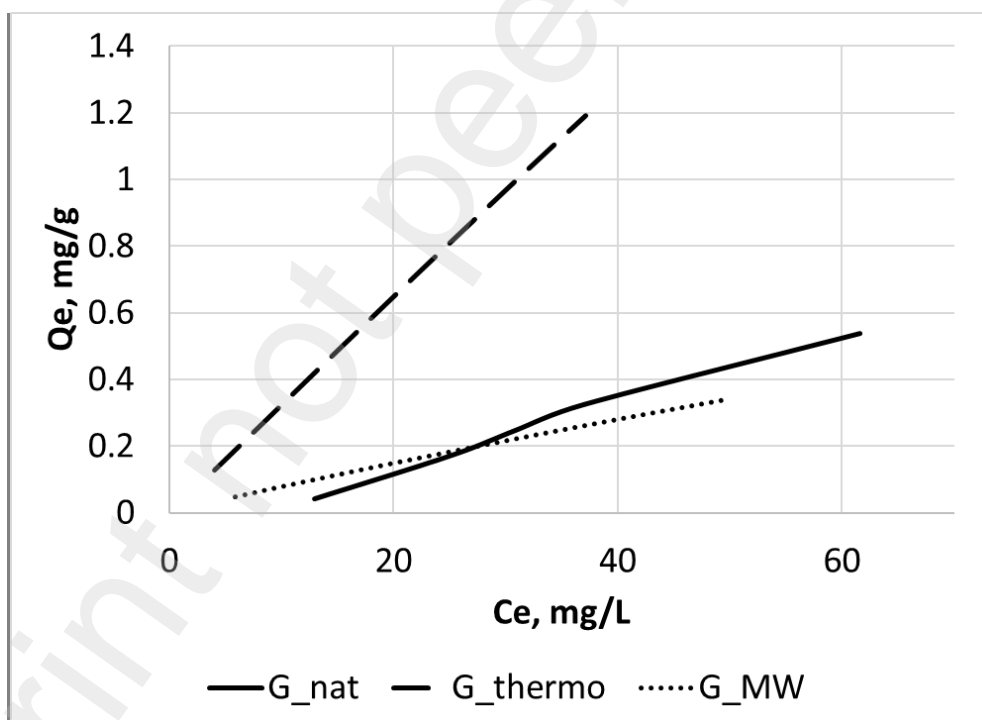


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Figure 6. Isotherms of NH_4^+ adsorption



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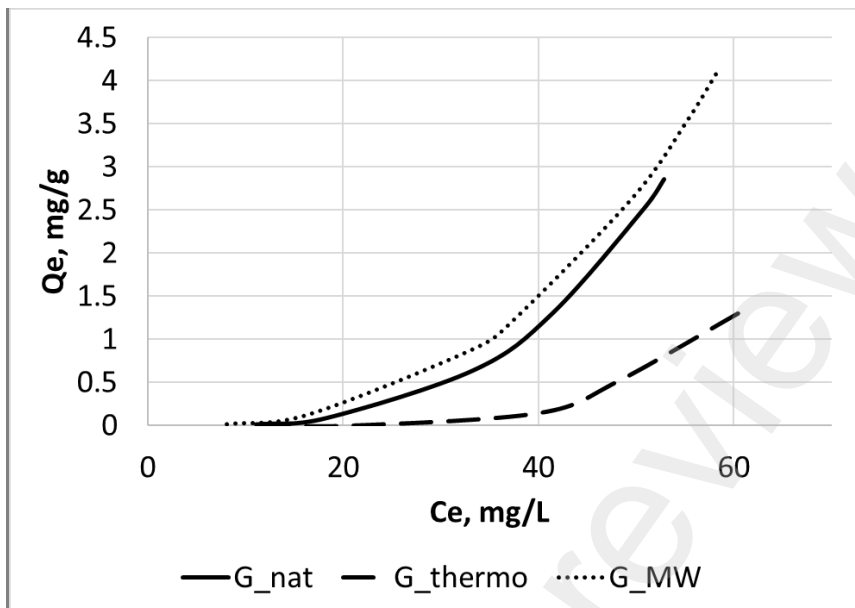
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Figure 7. Isotherms of PO_4^{3-} adsorption

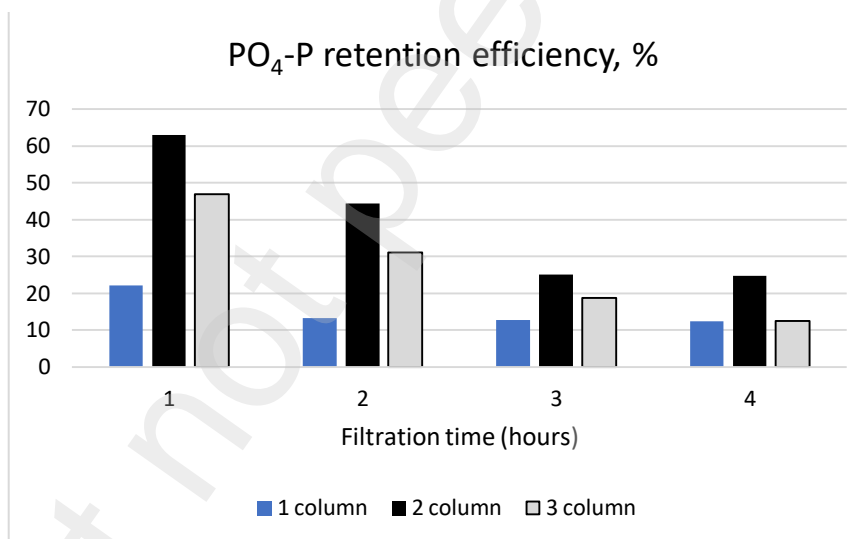


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Figure 8. $\text{PO}_4\text{-P}$ retention efficiency



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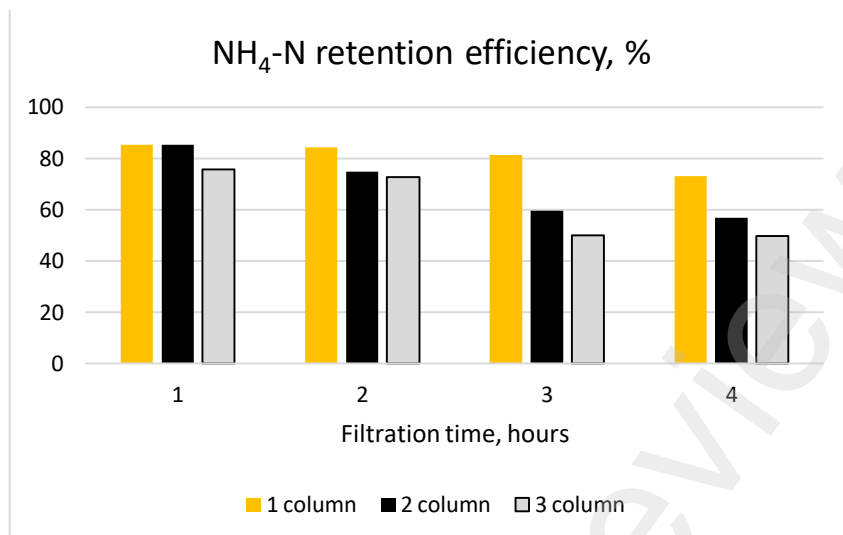
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Figure 9. NH₄-N retention efficiency



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572 **Table 1.** Specific surface area (S_{BET}), micropore area (S_{mic}), external surface area (S_{ext}), pore
 573 volume (V_p), equivalent particle size (d_{part}), and porosity (ϵ) of natural and modified clinoptilolite.

Sample code	S_{BET} , m^2/g	S_{mic}	S_{ext}	V_p , ml/g	d_{part} , nm	ϵ
G_nat	54.99	26.0	28.99	0.084	103.9	0.081
G_thermo	43.57	14.9	28.67	0.083	156.7	0.068
G_MW	50.28	20.1	30.18	0.086	107.3	0.087

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575 **Table 2.** NH_4^+ adsorption isotherms nonlinear fitting parameters.

	Sample index		
	G_nat	G_thermo	G_MW
Langmuir-Feundlich isotherm			
q_m	0.723	20.67	4.37
K_{FL}	0.025	0.0018	0.0015
n_{FL}	2.503	1.027	0.96
SNE	3.65	4.1	3.54
R^2	1.0	1.0	1.0
Dubinin-Radushkevich isotherm			
q_m	4.286	4.695	1.052
β	0.041	0.021	0.021
SNE	23.03	26.01	23.64
R^2	0.97	0.97	0.94
BET isotherm			
q_m	0.0012	236.29	115.95
C_{BET}	1.07	0.28	0.84
SNE	6.20	5.68	4.85
R^2	0.93	0.99	0.97

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Table 3. PO_4^{3-} adsorption isotherms nonlinear fitting parameters.

	Sample index		
	G_nat	G_thermo	G_MW
Langmuir-Feundlich isotherm			
q_m	113.58	1.78	101.21
K_{FL}	0.0062	0.0186	0.0055
n_{FL}	3.275	8.352	2.77
SNE	3.52	3.64	3.83
R^2	1.0	1.0	1.0
Dubinin-Radushkevich isotherm			
q_m	140	212.07	194.2
β	0.075	0.24	0.078
SNE	198.4	129.1	61.74
R^2	0.95	0.92	0.93
BET isotherm			
q_m	100.15	100.18	100.04
C_{BET}	0.01	0.0012	0.02
SNE	7.97	6.89	4.81
R^2	0.99	1.0	0.98

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